

**METHOD AND SYSTEM OF CONVERTING  
WASTE PLASTICS INTO HYDROCARBON OIL**

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**Field of the Invention:**

- 5 The present invention relates to a plastic oil extraction technology, and more particularly to a method of converting waste plastics into hydrocarbon oil, and a system for carrying out the same.

**Background of the Invention:**

- 10 The plastic oil extraction technology, or POET in short, has been used in processing solid wastes generated in urban areas and in industries. However, as noted in the research, it appears that there is still no practically applicable method and system of converting waste plastic into hydrocarbon oil. Most of the researchers in this particular field focus on the conversion of high polymer  
15 compositions into polymers of smaller molecules by utilizing thermal cracking of high temperature and high pressure, catalysts, while the operation platform used is either an oven type reactor or tubular type reactor. It is believed that the former reactor may be good for melting the solid plastics, but may not ensure the sufficient cracking, and discharge the residues efficiently, while the latter reactor is  
20 just opposite. The tubular reactor may efficiently discharge the residues of the cracking, but may not be suitable for processing directly the solid waste plastics.

- The plastic oil extraction technology of prior art usually includes thermal cracking, catalytic cracking, and cooling. One of the prior methods and systems is disclosed  
25 in EP 0 607 862 A. In order to obtain purified hydrocarbon oil, it utilizes a neutralization tank, in which the low-boiling hydrocarbon oil is subject to neutralization in a 20% sodium hydroxide aqueous solution, and an oligomerization tank, in which the cracking gas component is subject to oligomerization in a 100% phosphoric acid in addition to the aforesaid thermal,  
30 catalytic cracking and cooling. The other prior method or system is disclosed in WO 00/64997 of the same inventor, Mr. Tianfu JIANG. In that system, a subsidiary reactor is used to have the residues of the main thermal cracking reactor undergone a secondary thermal cracking so as to ensure the waste plastics fully gasified, and a heavy oil separator is used to recycle the heavy oil back to the

catalytic cracking reactor for further catalytic cracking.

However, the POET is aimed to process a mixture of hardly defined wastes plastics, containing many non-recyclable plastics, such as PP, PE, PVC, PET, PS, etc. in urban and industrial plastic wastes. Therefore, the conversion process from the solid wastes into a gaseous state can be hardly controlled. Thus, it creates lots of difficulties in the industrial application. This is probably the main reason why the plastic oil extraction technology has not been really put into practical use. The present invention is developed and perfected through many years of industrial research and practical testing. The present invention has solved the aforesaid difficulties, and thus can be readily adopted in the industrial application.

An object of the present system is to provide a method and system of converting the solid plastic wastes efficiently and thoroughly into pure and clean hydrocarbon oils of high calorie value up to about 11000 great calories per kilograms, and of a weight ratio of about 0.8. Such hydrocarbon oils can be used on any types of oil injection nozzle, and thus it can be widely used in the industry.

Another object of the present invention is to provide a system utilizing the combination of an oven reactor and a tubular reactor such that it can process various kinds of plastic wastes.

A still further object of the present invention is to provide a method and system of converting the solid plastic wastes into hydrocarbon oil without hazard hydrochloride.

### **Summary of the Invention**

In accordance with the present invention, a system of converting waste plastics into hydrocarbon oils comprises a thermal cracking reactor, into which solid waste plastics are fed and in which said waste plastics are cracked at a temperature in a range of 270-800°C to obtain a thermal cracking resultant of partly gaseous hydrocarbons, partly a mixture of liquid hydrocarbons and residues; a continuous thermal cracking and residual discharging portion connected to receive automatically the mixture of liquid hydrocarbons and residues from the thermal

cracking reactor, in which the liquid hydrocarbons are gradually and fully cracked into gaseous hydrocarbons when passing through the thermal cracking and residual discharge portion, while the dry residues from the previous thermal cracking and new residues generated from the further thermal cracking are discharged at a residual discharge outlet of the thermal cracking and residue discharge portion; a hydrochloride removal portion connected to receive the gaseous hydrocarbons, respectively, from the thermal cracking reactor and from the continuous thermal cracking and residual discharge portion; a catalytic cracking reactor being connected to the hydrochloride removal portion in which the gaseous hydrocarbons from the hydrochloride removal portion is subject to catalytic cracking with an acid catalyst; a cooling portion through which most of the gaseous hydrocarbons after the catalytic cracking are substantially converted into liquid hydrocarbons, and remaining non-convertible gaseous hydrocarbon substances are transported back to a burning chamber which compensates the heating of the thermal cracking reactor; and an pressurized activation reaction portion provided to receive the liquid hydrocarbons from the cooling portion to solidify few amount of sulfur nitrogen phosphorus contained in the liquid hydrocarbons so as to obtain purified hydrocarbon oils, thereby reducing the generation of SO<sub>x</sub> and NO<sub>x</sub>.

The thermal cracking and residual discharge portion consists of continuous thermal reacting tubes of parallel arrangement. A mixture of the melting waste plastics and other impurities, that is, liquid hydrocarbons and residues, is pushed forward by screw conveyors mounted inside the tubes, and thus passes through the thermal reacting tubes, while the mixture is maintained at a high temperature sufficient to enable further gasification of the melting wastes plastics, or rather liquid hydrocarbons, to ensure the sufficient thermal cracking of the gaseous hydrocarbons.

The hydrochloride removal reaction of the present invention is to have the thermal cracking resultants, i.e., gaseous hydrocarbons, in reaction with alkaline substances to replace the chlorine from hydrochloride contained in the thermal cracking resultants so as to obtain purified gaseous hydrocarbons. The hydrochloride removal reaction is at a high temperature. After the reaction, the

gaseous hydrocarbons are almost hydrochloride free.

The cooling portion of the present invention consists of three stages of cooling, whereby gaseous alkene of large molecules will be substantially converted into gaseous alkene of small molecules, such as eight to twenty carbon atoms, and eventually become liquid hydrocarbons, leaving only few non-convertible gaseous hydrocarbon substance, that is, non-convertible at room temperature and pressure. Such non-convertible gaseous hydrocarbon substances will be sent back to the burning chamber for the thermal cracking reactor to compensate the heating supply for the thermal cracking reaction.

### **Brief Description of the Drawings**

Fig. 1 is an illustration of a system in accordance with the present invention;  
Fig. 2 illustrates the structure of the continuous thermal cracking and residual discharge portion of the present invention; and  
Fig. 3 is an illustration of the structure of the chlorine removal portion.

### **Detailed Description of the Invention**

The raw waste materials are usually urban and industrial waste plastics, that normally contain many non-recyclable plastics, such as PP, PE, PVC, PET, and PS, etc. For recycling those waste plastics, some kinds of pretreatment may be required. Usually, such waste plastics are sorted roughly at individual homes or wastes collection sites before they are brought to a recycling plane. At the recycling plane, the waste plastics are subject to separation by one or more separator. There are normally magnetic selection separators and air-blowing selection separators. The magnetic selection is primarily for separating the relatively big metal wires, or other metal parts, while the air-blowing (or wind) selection is primarily for separating dust or dirt contained in the wastes, and reducing water contents.

After the pretreatment, the waste plastics are sent to the system of the present invention. Such a system usually contains a material feeding system (not shown) to prevent the feeding materials from spilling out, and prevent the gas seepage from the reactors to avoid any ignition of burning and explosion. The feeding

system may use an automatic piston of hydraulic pressure control that does not require crashing the waste materials, or use a screw-propelling feeding system that requires crashing the wastes materials before feeding. The latter system may reduce the dust or dirt in the processed waste materials.

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Then, the waste plastics enter the thermal cracking reactor **11** through the feeding system at the feeding entry **1** with reference to Fig. 1. The thermal cracking reactor **11** is an oven type reactor, and it is a cylindrical and sealed container made of titanium steel. The outside of the thermal cracking reactor **11** is normally provided with a heating furnace sleeve (not shown) and an automatic ignition system (not shown) in association with the heating furnace. The temperature inside the thermal cracking reactor is controlled at 270-800°C, and the pressure inside the oven reactor is the environmental atmosphere or pressure. Once the waste plastics get into the reactor, they start the thermal cracking reaction at 270-800°C, and the molecule chains of the plastics are gradually broken. The practical test shows that 30% of the solid waste plastics become gasified soon after they become liquid in the thermal cracking reactor **11** at a matter of few seconds. Thus, the thermal cracking resultants are about 30% gaseous hydrocarbons, as well as about 70% of a mixture of non-gasified liquid hydrocarbons substances and other residues, that is, melting waste plastics.

As shown in Fig. 1, the mixture of gaseous hydrocarbons substances and residues, the melting waste plastics, are led from the thermal cracking reactor **11** to a hydrochloride removal portion **13**, while the melting waste plastics are passed to the continuous thermal cracking and residual discharging portion **12** that is a tubular thermal reactor. In the 70% melting plastics are mixed of various impurities, such as carbonized material and dirt etc. These melting plastics pass uniformly through the heated continuous thermal cracking and residual discharging portion that consists of several sets of reacting tubes of acid resistant, i.e., so-called tubular type of reactor. This portion also functions as a residual discharging system. During this process, the inside temperature of the reacting tubes is maintained at 270-800°C to ensure fully thermal cracking reaction.

With reference to Fig. 2, the tubular thermal cracking and residual discharging

portion **12** comprises a plurality, such as five or six, sets of steel tubes **3** of predetermined length that are parallel arranged. The screw propellers or conveyors **20** mounted inside the steel tubes rotate at opposite directions in adjacent tubes, and the entire portion **12** is placed within a heating sleeve with a temperature at 270-800°C. The metal screw propellers or conveyors propel the melting plastics forward such that the 70% melting plastics pass the heated tubes and the residues enter the residual discharging system. As accurately calculated, the length of the tubes **3** and the rotation speed are set such that the melting liquid plastics pass the whole system at a predetermined speed such that the melting plastics are fully gasified before reaching to the end of the continuous thermal cracking and residual discharging portion **12**, and the gaseous thermal cracking resultants are led out of a gas outlet **4** to the hydrochloride removal portion **13**. The impurities in the melting plastics become powder substances to be eventually discharged at the other outlet of the continuous thermal cracking and residual discharging portion. The stability and continuity of the industrial production are maintained by the continuous and constant feeding of the materials.

The hydrochloride removal portion **13** of the present invention is shown in Fig. 3. The art used here is different from the dry or damp neutralization method currently used in the industry. This is a new technology of hydrochloride removal at high temperature, whereby the existence of hydrochloride in the gaseous hydrocarbons is minimized or almost eliminated. The catalysts are made of several alkaline compounds and heavy metal elements to form metathetic substances, and they are reusable so as to increase the side products, chlorine gas ( $\text{Cl}_2$ ), and reduce the cost.

In the gaseous hydrocarbons of high temperature generated from the thermal cracking reactor and the continuous thermal cracking and residual discharging portion, there could be certain amount of hydrochloride ( $\text{HCl}$ ). As studies show, there are about 5-15% plastics among the urban solid wastes, and about 5% of the plastic wastes are PVC. The PVC materials are hard to be separated from other plastic wastes, if mixed, and the PVC will generate  $\text{HCl}$  through thermal cracking. The aforesaid gaseous hydrocarbons pass the acid-resistant pipelines. The temperature of the hydrochloride removal system **13** is maintained at 270-

800°C. Because of the effect of the metathetic substances, the gaseous hydrochloride in the gaseous hydrocarbon substances will become solidified rapidly so as to ensure that the amount of hydrochloride in the gaseous hydrocarbons is almost zero, i.e., almost hydrochloride free.

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As shown in Fig. 3, the gaseous hydrocarbons and the mixed few amount of hydrochloride pass the pipeline 2 (Fig. 1), and enter the hydrochloride removal portion 13. Then they react with the specific metathetic substances 26 under the condition of a temperature of 270-800°C to have the chloride ion solidified to form compounds. Other gaseous hydrocarbon substances will enter through a pipe 10 into a setting bed 22. The outer portion 23 of the hydrochloride removal portion 13 is a heating sleeve, provided to maintain the condition of removing hydrochloride, i.e., the high temperature. As accurately calculated, it is possible to have the metathetic substances saturated within a predetermined time interval. In this case, the pipeline 2 can be switched to another identical hydrochloride removal portion. The reaction state is the same as that discussed above.

At the same time, the first hydrochloride removal portion receives hot air through the pipeline 21 to react with the metathetic substances. The chlorine element contained therein will be replaced and changed into chlorine gas, and then expelled, through the pipe 24, together with the hot air out of the hydrochloride removal portion 13. Then, the expelled gas enters the chlorine separation system to collect chlorine gas.

Upon leaving the hydrochloride removal portion 13, the gaseous hydrocarbons enter a catalytic cracking reactor 14. The gaseous hydrocarbons of high temperature, under the effect of a special catalyst, will be rapidly cracked again into gaseous hydrocarbons substances of much smaller molecule compositions. More specifically, the catalyst can be repeatedly used to reduce the cost.

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The cooling portion of the present invention includes a three-stage cooling and condensing 15, 16, 17. The gaseous hydrocarbons coming out of the catalytic cracking portion have undergone the cracking reaction twice, respectively, in the thermal cracking reaction and the catalytic cracking reaction. The big molecules of

the gaseous hydrocarbons may have been completely broken up so as to obtain gaseous hydrocarbon of smaller molecules, such as eight to twenty carbon atoms. Then, after the three-stage cooling and condensing, about 85-90% of the gaseous hydrocarbons become liquid hydrocarbons, i.e., hydrocarbon oils, while the remaining substances will pass through the pipelines **6, 7, 8** (Fig. 1) and be lead, through a LPG recovery system, into a burning chamber (not shown) to compensate the heating of the thermal cracking reactions. The aforesaid remaining substances are non-convertible hydrocarbon substances that can only be gaseous under the normal temperature and pressure, such as methane, butane, etc.

The system of the present invention further includes a pressurized activation reactor **18**. This reactor provides 0.8-1 atmosphere and normal temperature as the reaction conditions, and adds special additives to enhance the fluidity of the hydrocarbon oils, to have the hydrocarbon oils further cracked (cold cracking), and to increase the calorie value of the resulting hydrocarbon oils. In the meantime, due to the effect of the additives, a small amount of sulfur, nitrogen, phosphorus elements contained in the liquid hydrocarbons are solidified so that the resulting hydrocarbon oils become highly purified. A high-speed centrifuge **25** may be adopted to extract the purified hydrocarbon oils (Fig. 1).

The method of the present invention is described hereinafter. The waste plastics are fed into the thermal cracking reactor **11** through the material entry **1**. The thermal cracking reaction is carried out in an oxygen free environment, at a temperature of 270-800°C, and under the environmental atmosphere pressure. It is confirmed that about 30% of the solid waste plastics become gaseous products soon after they become liquid. Then, the thermal cracking resulting gas passes through the pipeline **2** and enters into the hydrochloride removal portion **13**.

The remaining 70% melting liquid plastics in the thermal cracking reactor **11** are mixed with impurities, and pass through a control valve (not shown) at the bottom outlet of the thermal cracking reactor **11**, entering into the continuous thermal cracking and residual discharging portion **12**. The melting plastics flow gradually through the tubes **3** (Fig. 2) of the continuous thermal cracking and residual



discharging portion **12**. There, the melting liquid plastics are further thermally cracked, and become gasified. The thermal cracking resulting gaseous hydrocarbon substances enter the hydrochloride removal portion **13** through the pipeline **4**.

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With the completion of the gasification at the end of the continuous thermal cracking and residual discharging portion **12**, the dry residuals are expelled through the metal screw conveyors **20** inside the tubes **3**. Through the pipelines **2** and **4**, the gaseous hydrocarbon substances after the thermal cracking enter into the hydrochloride removal system **13**. The special metathetical substances will capture the chloride ion of the gaseous hydrochloride to generate chlorine gas. The resulting chlorine gas is expelled out of the removal portion **13**. Then, the gaseous hydrocarbons are almost hydrochloride free. The gaseous hydrocarbons substances pass through the pipeline **5** and enter the catalytic cracking reactor **14**.  
10 In the catalytic reactor **14**, the gaseous hydrocarbons are catalytically cracked under the effect of an acidic catalyst to become light groups of gaseous hydrocarbon substances of small molecules. Then, the catalytic cracking resultants enter the three cooling and condensing stages **15**, **16**, **17** to obtain liquid hydrocarbons of small molecules.

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When the gaseous hydrocarbon substances pass the through three cooling stages, any gaseous hydrocarbon substances, that may become liquid hydrocarbons, will change into the liquid hydrocarbons. These are the basic extracted oil components. Most of them, however, are unsaturated alkene substances. At the normal temperature and pressure, the still gaseous hydrocarbons substances are non-convertible LPG. These non-convertible gaseous hydrocarbons or LPG will be led through the pipelines **6**, **7**, **8** and LPG recovery system back to the burning chamber for the thermal reaction or return to the heating furnace sleeve of the thermal cracking reactor **11** to compensate the  
25 heating capacity.  
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The collected liquid hydrocarbons pass through the pipeline **9** and an oil pump (not shown), and then enter the activation reactor **18**. Under the reaction condition of 0.8-1 atmospheres, a special industrial additive is added into the activation reactor

18. There, few amount of sulfur, nitrogen, phosphorus elements contained in the liquid hydrocarbons become solid, while the liquid hydrocarbons get further cracked (cold cracking) to increase the percentage of the saturated hydrocarbons. Then, these saturated hydrocarbons become purified and clean light hydrocarbon oils of high fluidity and high calorie value.

In accordance with the present invention, the removal of hydrochloride is carried out at a high temperature. It is believed that such hydrochloride removal is not known before, that is, removing hydrochloride at a high temperature, for instance, 270-800°C. The hydrochloride mixed in the gaseous hydrocarbons of high temperature forms an acidic mixture of high temperature. The hydrochloride is removed first to ensure that the gaseous hydrocarbons enter the setting bed (molecule sieve) safely without damaging the catalyst therein. Here, the metathetic substances can be recycled for repeated use to reduce the cost.

The conventional technique of hydrochloride removal is based on dry method or damp method. The principle is the neutralization of acid and alkaline. Such a method would require a large amount of calcium oxide in case there is a large amount of hydrochloride. At the same time, it would generate a large amount of calcium chloride. Therefore, in practice, it may create some troubles during the transportation, additional resultants, and other technical treatment difficulties. Thus, it would increase the operation cost.

When removing hydrochloride at a high temperature, the specific catalyst may replace the chlorine through certain oxidation after it absorbs the chloride ion. Thus, it not only reduces the operation cost, but also avoids the generation of the large quantity of useless inorganic salt. Further the cost may be reduced because there is no large amount of alkaline neutralizers required, and no need to deal with the large amount of generated inorganic salt. Moreover, there is no useless resultant. The resulted chlorine gas is still of marketable value.

The scope of protection of the present invention is set out in the following claims. However, any obvious modification without excess of essence of the present invention should also be within the scope of the present invention.